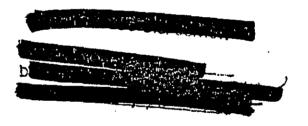
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AN INVESTIGATION OF EFFLUENT CONTROL STANDARDS AND PRACTICES

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SEPTEMBER 1967



TABLE OF COLTECTS

			PAGE NO.
LIST OF TA	ABLES		£
LIST OF I	LLUSTRATIO	NS	11
SECTION			1-33
ı.	INTRODUCT	ION	1
II.	SUMMARY-		2-3
III.	AUTHORITA	TIVE STANDARDS	3- 5
IV.	EFFLUENT :	SOURCE IDENTIFICATION	5-13
v.	CONFORMAN	CE WITH EFFLUENT CONTROL STANDARDS	14-32
VI.	RECORDS A	ND REPORTING	33
VII.	ACKNOWLED	GEMENTS	33
LIST OF RE	Ferences .		34
APPENDICES			35-65
Append		EXECUTIVE ORDER 11288, PREVENTION, CONTROL, AND ABATEMENT OF WATER POLLUTION BY FEDERAL. FACILITIES	35–38
Appeni	DIX II	FROPOSED WATER QUALITY STANDARDS FOR INTER- STATE AND COASTAL WATERS FOR THE STATE OF WASHINGTON AND A PLAN FOR IMPLEMENTATION AND ENFORCEMENT OF SUCH STANDARDS	39-47
APPENI	OIX III	SUMMARY - BACTERIOLOGICAL, PHYSICAL, CHEMICAL AND RADIOACTIVITY LIMITS OF THE DRINKING WATER STANDARDS, 1962	48-52
APPEND	OIX IV	DESCRIPTION - 300 AREA PROCESS POND EFFLUENT SAMPLER	53
APPEND	OIX V	EXECUTIVE ORDER 11282, PREVENTION, CONTROL, AND ABATEMENT OF AIR POLLUTION BY PEDERAL ACTIVITIES	54-59
APPEND	IV XI	TENTATIVE HANFORD AIR QUALITY GUIDE	60
APPEND	OIX VII	OCCUPATIONAL THRESHOLD LIMIT VALUES OF COMMONLY USED CHEMICALS IN THE PRODUCTION FUELS SECTION -	61
APPEND	IIIV XIC	SCHEMATIC DIAGRAMS - 313 and 306 BUILDING	60.65

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LIST OF TABLES

TABLE	•	PAGE NO.
I	FUEL AND CHEMICAL STORAGE	5
II	LIQUID EFFLUENTS DISCHARGED TO THE PROCESS SEWER	7-9
III	GASEOUS EFFLUENTS DISCHARGED TO THE ATMOSPHERE	13
IA	RANGE OF TYPICAL CONTAMINANTS, 300 AREA PROCESS POHD INLET AND EAST BANK	15
Y	NORTH PROCESS POND ANALYSES	16
VI	BANK SEEPAGE ANALYSES	17
VII	TYPICAL RADIOCHEMICAL ANALYSIS OF ANODIZING CAUSTIC SOLUTION	25
VIII	TYPICAL RADIOCHERICAL ANALYSIS OF WELL 399-1-1 AND BANK SEEPAGE BAMPLES	25-26
IX	BACTERIOLOGICAL ANALYSIS OF LEACHING TRENCHES, WELLS, AND COLUNBIA RIVER	26

LIST OF ILLUSTRATIONS

Figure		PAGE NO.
1.	CHEMICAL STORAGE TARKS AND TRANSFER LINES	6
2.	DUN 300 AREA PROCESS SEMER LINES	io
3.	DIN CONTAMINATED SENER LINES	11
L.	SANITARY SHWER SYSTEM	12
5.	Cr+6 ANALYSES - PROCESS POND INLET	18
6.	cr ⁺⁶ analyses - East Bank and River Bank Seepage	19
7.	NO3 ANALYSID - PROCESS POND INLET	20
8.	NO3 ANALYSES - EAST BANK AND RIVER BANK SEEPAGE	21
9.	URANIUM ANALYSES - POND INLET AND RIVER BANK SEEPAGE	22
10.	URAMIUM AMALYGES - EAST BANK AND RIVER BANK SEEPAGE	23

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AN INVESTIGATION OF EFFLUER CONTROL STANDARDS ALD PLACTICES

INTRODUCTION I.

In conjunction with the increased emphasis being placed on air and water effluent quality within Federal facilities, it became necessary to investigate the various aspects of effluent control responsibilities applicable to the Production Fuels Section. impetus to the study, a recent RL-AEC Waste Disposal Inspection Report of Douglas United Huckear (Reference 5) recommended that nonradioactive chemical releases to 300 Area laguons be analyzed to assure compliance with accepted release standards.

The task at hand was to assemble the various authoritative standards, investigate current practices, compare these practices with accepted standards, and establish a responsive effluent control program aimed at continuing compliance with these standards.

Effluent control practices were compared with the following release criteria supplied by the Federal and State Covernments:

- Executive Order 11288, "Prevention, Control, and Abatement of Water Pollution by Federal Activities," dated July 7. 1966
- Proposed Washington State Quality Standards for Interstate and Coastal Waters," dated June 5, 1967
- Executive Order 11282, "Prevention, Control, and Abatement of Air Pollution by Federal Activities," dated May 26, 1966
- Tentative Hanford Air Quality Gunde (to be issued)
- RL Manual Appendix 0510, Part I, "Radioactive Waste Disposal Guides." dated July 13, 1967

Copies of these standards can be found in the Appendices of this report.

It is trusted that the information contained herein will serve the dual purpose of providing the necessary inputs to those immediately responsible for pollution control and informing others of the current effort being made to assure continuing compliance.

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II. SUMMARY

A. LIQUID EFFLUENT CONTROL

This investigation showed that the chemical and sanitary offluents being released by the 300 Area contractors to the process pends and septic tanks do not contribute a significant amount of pollution to the environs. This conclusion is based on the results of a comprehensive sampling survey of the north process pend, Columbia River bank seepage, leaching trenches, and the Columbia River.

Current storage facilities for liquid chemicals as presently located would not contribute a significant amount of water pollution in the Columbia River should a rupture or accidental drainage occur.

Operating procedures are available involving the receiving, storing, and distributing of liquid chemicals and their subsequent use in the production process. These procedures provide a comprehensive summary of the methods utilized in controlling the various production process variables.

Future action planned in order to assure continuing compliance includes the gathering of effluent samples by an automatic effluent sampler at the process pend inlet. Chemical and radio-chemical analyses will be periodically performed. Grab samples will be taken from the wells in the vicinity of the pends, along with Columbia River bank seepage samples, to assess the amount of contaminants in the ground water. Samples from the leaching trenches and Columbia River will continue to be taken and analyzed for Biochemical Oxygen Demand (BOD) and coliform content by Battelle-Northwest.

B. GASEOUS EFFLUENT CONTROL

The results of a survey of the Production Fuels Section powerhouse stack by NEMF were inconclusive because of the difficulty in obtaining a representative sample. Additional studies are scheduled to be initiated during the winter months when high steam generation rates are expected.

Smoke density measurements indicate compliance with the standards. The recommendation from HEHF regarding the type of smoke alarms for monitoring the ecabustion units is pending until a reply to an inquiry to the Department of Health, Education, and Welfare is received by the AEC.

The disposal of refuse that can be burned in open pits does not comply with the 25-pound-per-day limit. Because of the remote location, low population density, and favorable meteorological conditions, it is believed that the standard is unduly restrictive; and an exemption has been requested by the AEC. Special disposal precautions will be used should significant quantities of dark-smoke-producing refuse be accumulated.

HEHF is scheduled to procure air monitoring equipment in October, 1967, and will monitor selected locations in the 300 Area to determine if the Production Fuels Section's gaseous effluents are harmful. Until that time, no change in the current mode of operation is contemplated.

III. AUTHORITATIVE STANDARDS

A. LIQUID EFFLUENCE (KONPADIOACTIVE)

Executive Order 11288, deted July 7, 1966, outlines the necessary Federal government policy and requirements that are applicable to Federal agencies and the Atomic Energy Commission and its contractors in regard to the prevention, control, and abatement of water pollution. Detailed copies of this correspondence are included in Appendix I.

In addition to Executive Order 11288, the Production Fuels Section is expected to comply with the water quality standards as established by the state of Washington. Hearings were held in Olympia on June 6, 1967, regarding a proposal before the Pollution Control Commission for the adoption of water quality standards for interstate and coastal waters of the state of Washington, and a plan for implementation and enforcement of such standards.

In the proposed standards, the Columbia River has been categorized in Class A from the mouth to Grand Coulee Dam. Water quality criteria applicable to this classification are listed in Appendix II.

B. GASEOUS EFFLUENTS (NONRADIOACTIVE)

Executive Order 11282, dated May 26, 1966, outlines the necessary Federal government policy and requirements that are applicable to Federal agencies and the Atomic Energy Commission and its contractors in regard to the prevention, control, and abatement of air pollution. Detailed copies of this correspondence are included in Appendix V.

As an initial attempt to satisfy the intent of Executive Order 11282, tentative Air Quality Guides for the Hanford Plant have been established (Appendix VI). These limits, generated by representatives of the Hanford contractors and the Richland Operations Office of the AEC, would apply at the boundaries of the reservation and are based on 1/10 of the Occupational Threshold Limit Values (See Appendix VII). The Threshold Limit Values refer to air-borne concentrations of substances and represent conditions under which it is believed that nearly all workers may be repeatedly exposed, day after day, without adverse effect. Selected monitoring of the mir within the plant boundaries will be the responsibility of HEHF. After locating the source of the pollutant, it is expected that specific building and process effluent release standards will be developed in the future to reduce the concentration of those pollutants which exceed the standards.

In addition to Executive Order 11282, the AEC in a letter dated April 21, 1967, directed that no rubber, tar, petroleum or other dark-smoke-producing materials be burned in open pits.

C. RADIOACTIVE RELEASE CRITERIA AND PROCEDURES

The release and control of solid, liquid, and gaseous, radioactive wastes is described in Sections D, E, and F of RL Appendix 0510 and will not be covered in detail in this document. Certain limits involving liquid and gaseous releases, however, were extracted and are listed below.

1. Liquid Radioactive Wastes (Open Pond Disposal)

"Liquid wastes discharged to large, open ponds should be essentially free of radioactive materials. Concentrations of 5 X 10⁻⁵ µci/ml (low level) should not be routinely exceeded. In the event this concentration is exceeded, control should be established to evaluate the likelihood of its becoming an environmental contamination problem. Liquid wastes failing to meet this criteria should be transported to the 200 Area underground disposal facilities."

2. Gaseous Radioactive Wastes

"The guides for effluent release from each stack in the 300 Area are:

92125879318

	Release Gu	ide (curie/week)
Radionuclides	150-foot Stack	Short Stack or Vent
Sr90	5 X 10 ⁻²	1 x 10 ⁻²
I131	5 X 10-1	2 x 10-1
Pu (total)	5 x 10 ⁻³	1 x 10 ⁻³
U (natural)	2 X 10 ⁻²	4 x 10 ⁻³
Total of others except H3, C14, and Noble gases	10	2

IV. EFFLUENT SOURCE IDENTIFICATION

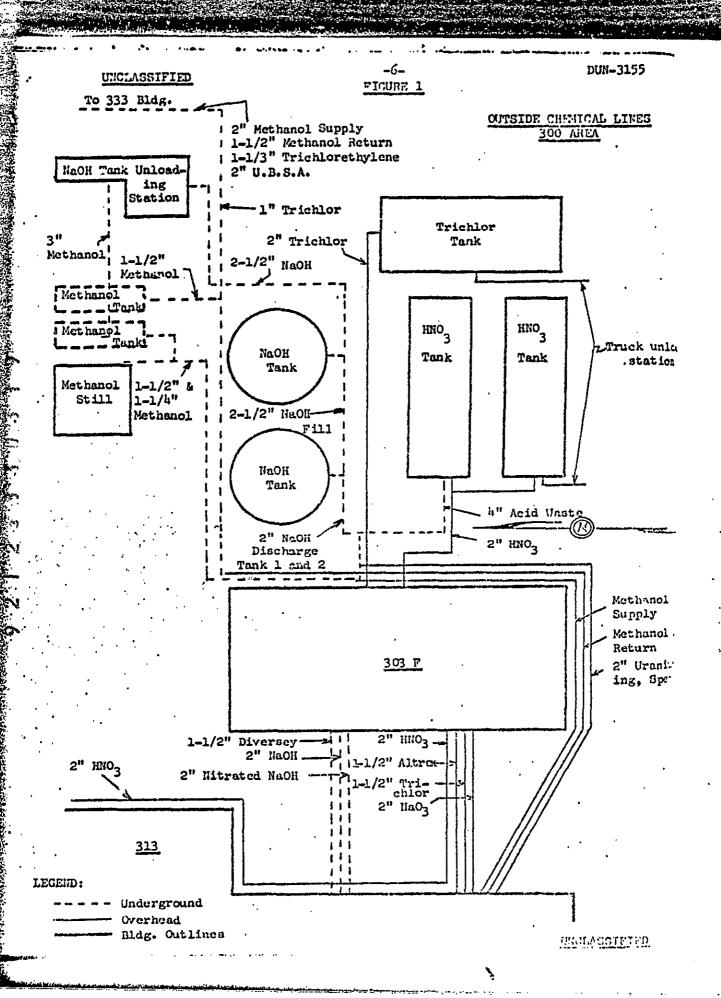
A. LIQUID EFFLUENTS

1. Chemical Storage

Outside storage tanks that supply the necessary process chemicals for the Production Fuels Section are listed along with the inventory value in Table I. Methanol, trichlorethylene, nitric acid, and sodium hydroxide are distributed by various pumping mechanisms through the 303-F Building. A schematic diagram of the location of the tanks and transfer lines is shown in Figure 1. For safety purposes, the methanol tanks are buried. Batch quantities of nitrated-caustic, deoxidizer, and Altrex are pumped after mixing in 303-F.

TABLE I
Fuel and Chemical Storage

Chemical	Storage Capacity	Inventory Value
HNO ₃	2 - 4,000 gal. tanks	\$ 1,600
NaOH	2 - 10,000 gal. tanks	4,000
Trichlorethylene	1 - 10,000 gal. tank	10,900
Methanol	1 = 6,000 gal. tank 1 = 4,000 gal. tank	3,000
Puel Oil	2 - 75,000 gal. tanks 1 - 15,000 gal. tank	10,500 1,050 UNCLASSIFIED



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2. Process Solutions

Table II lists the chemicals that are routinely discharged in significant quantities from the 313 and 306 buildings. A portion, if not all, of these eventually reach the Columbia River through underground scepage from the process ponds. The drainage of these chemicals flows through process sever lines to the pends as shown in Figure 2, with alternate use of the north and south pends being made. The empty pend is scarified before being reuced. Approximately 5.5 million gallons of effluent water is discharged daily from the total 300-Area operation which includes DUN and Battello contributions. Pend operation and maintenance is the landlord responsibility of DUN.

Cck uni

TABLE II Liquid Effluents Routinely Discharged to the Process Sewer

313 Building - Component Preparation

do.				Concentration	
' /3	- tation	Chemical Q	uantity (gal)	(155/Sal)	Dumping Frequency
<u> </u>	Sleeve Machine	NaOH	800 -	2.2 - 3.3	2 Weeks
;	Siceve Machine	Ivory . Scap	50	0.1	Twice Daily
N	Sleeve Machine	NaAlO ₂	100	0.03 - 0.07	Daily
thanol Oply chanol	Cap & Can Nurning	Cleaner	1080	0.19 - 0.34	36 Line-days
Urani:	Car & Can Machine	Deoxidizer ⁻²	710	1.25 - 2.5	72 Line-days
g, Spc:	Spire Etch	(MaOH (NaNO ₃ (Chelating Agent ⁻³	300 300 300	0.26 - 0.55 0.20 - 0.60 0.035 - 0.120	Twice Weekly Twice Weekly Twice Weekly
	· or	Aluminux ⁻¹	300 .	0.26 - 0.55 (NaOH content)	Twice Weekly
	Spire Etch	нио3	150	0.4 - 1.4	Weekly
	Special Products	Aluminux ⁻⁴	100	0.26 - 0.55 (NaOH content)	As Necessary
<u>{</u>					nclassified

313 Building - Component Preparation (continued)

Yanahim	(The maine)	Quantity (gal)	Concentration (lbs/gal)	
Location	Chemical			Dumping Free.
Special Products	NaNO3	300	0.33	Every Other :
Special Products	Deoxidizer ²	300	0.80 - 1.88	As Necessary
Tool Cleaning	NaOH	203	2.5	Weekly
	<u>313</u>	Building - Recovery	•	
Stripper Tank	NaOH NaOH	300 100 pounds per 225 pieces		12 Times Mont:
Filter Press	NANO ₃ Uranium (Negl)	2241	Unknown 4 lbs/month	Continuous When Running
	313 B	uilding - Anodizing	,	
Plating Tanks	H2C204 2H2O	2 - 425	0.51 - 0.68	Infrequently
Cleaning Tank	NeNO3 NeOH	125	ز.0	2 Weeks
	313 3	uilding - Finishing	•	
Etch Machine	нио3	1500	1.4 - 3.0	2-4 Months
·	<u>313 Bu</u>	ilding - Slug Pickl	<u>e</u>	
Pickle Rinse	Uranium	2000	About 60 lbs. per month	Continuous
		306 Building		
Hand Cleaning Line	Aluminum ⁻⁴ NaNO ₃	100	0.26 - 0.55 0.20 - 0.40	6 Per Month
Hand Cleaning Line	Deoxidizer	60 ·	0.80 - 1.20	2 Weeks
Automatic Cleaning	нчо ₃ Иеон	80 55	5.0 5.0 - 6.0	2 Weeks Every Other it
Autometic Cleaning	нио3	80	2.5	Twice Monthly
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TABLE II (continued)

Carrosition consisting mainly of:

Cleaner:

Deoxidizer:

Na₂CO₃, Na₂SiO₃, Na₄P₂O₇

r Da

NaHSOh, Croz or NagCroz, NagSiF6

ry

anti-

Chelating Agent: NaCcH1107 (Sodium Cluconate)

Aluminux:

NaOH, NaC6H1107

: onth:

.r Day

hly

3. Contaminated Effluents

Contaminated wastes from Battelle facilities are routinely discharged to storage tanks at the 340 retention and neutralization building as shown in Figure 3, and are later transported to the 200 Areas for disposal. Waste destined for the process pond is held in storage basins, sampled, and then released. Except for an occapional spillage, Battelle does not contribute a sign: leant quantity of radioactivity to the process ponds.

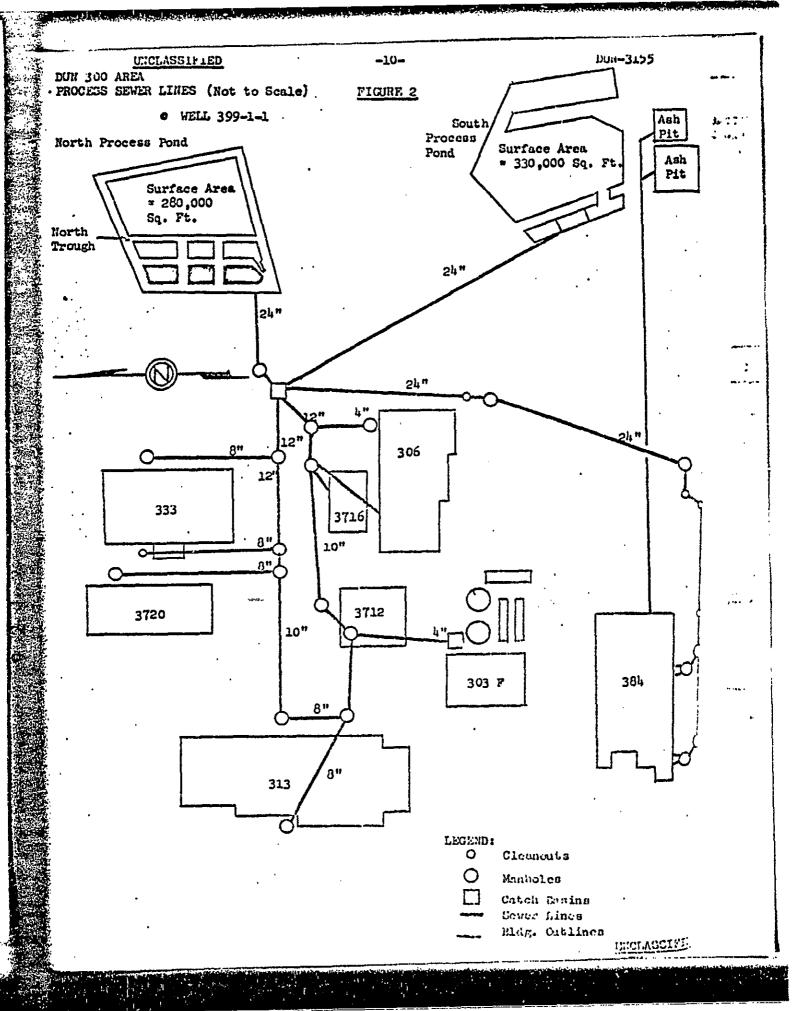
Normal and enriched uranium are discharged from waste solutions from DUN 300-Area operations. In FY 1967, approximately 245 pounds of enriched and 525 pounds of normal uranium were discharged, according to accountability figures, from the Production Fuels Section while the N-Fuels contribution totaled approximately 1,000 pounds.

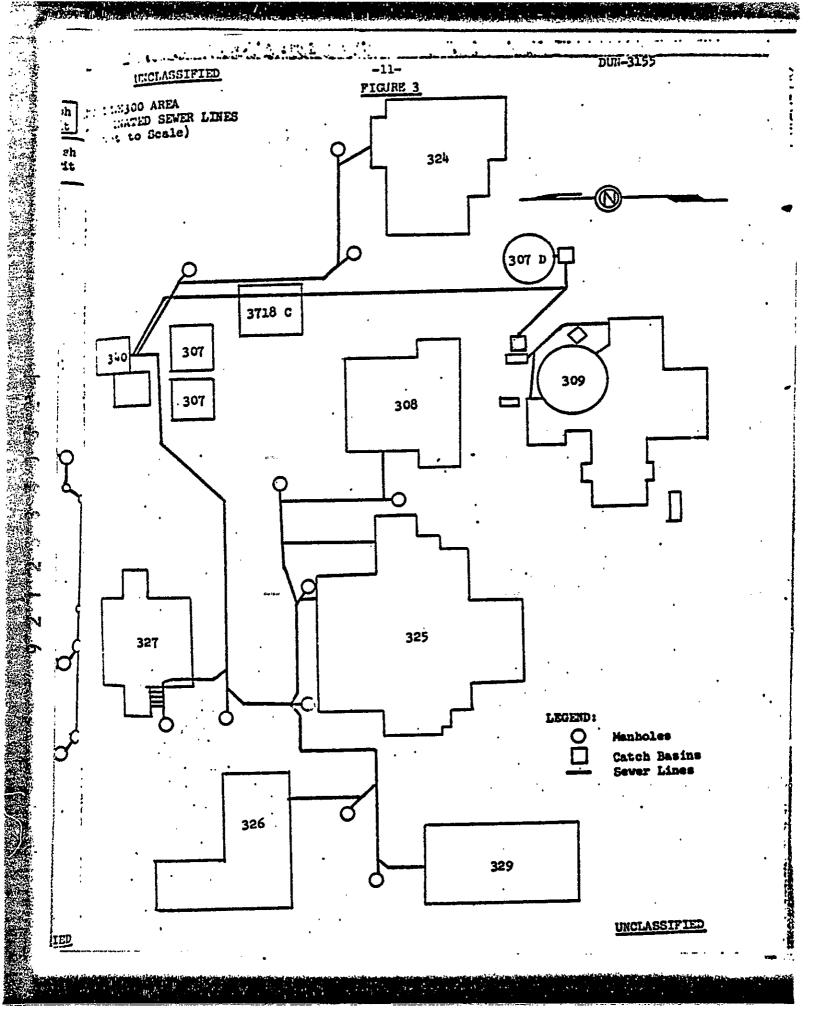
The anodizing process contributes certain radioactive activation products from the caustic cleaning solution in 306 Building. Garma scans have shown the presence of Zn65 Zr-Nb, Se⁴⁶, Fe⁵⁹, Co⁶⁰, and Co⁵⁸.

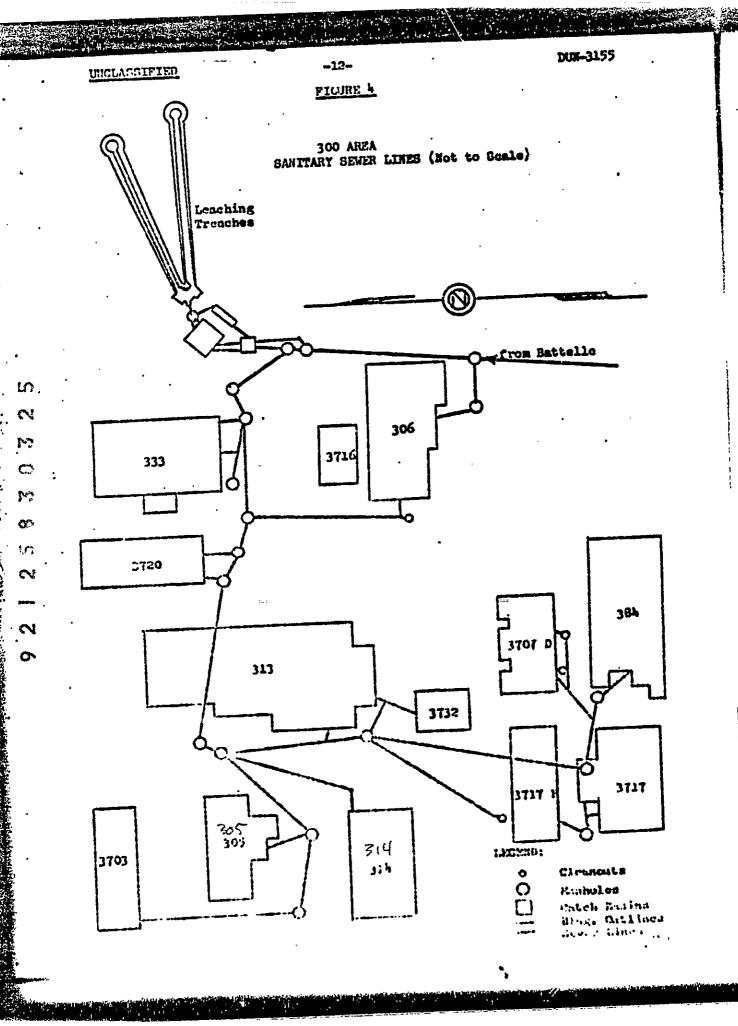
4. Sanitary Wastes

One common sanitary waste disposal system serves all 300 Area contractors and is the operational responsibility of DUN.

Sewage flows through vitreous tile pipe to septic tanks, and the daily overflow of approximately 300,000 gallons per day drains into one of two 500-foot long leaching trenches. The · septic tanks are periodically cleaned and the solids disposed into a sludge pit located near the leaching trenches. A schematic diagram of this disposal facility is shown in Figure 4.







B. GASPOUR PEFLUEPTS

Gaseous effluents that are routinely discharged to the atmosphere from the Production Fuels Section facilities are listed in Table III.

TABLE LIL

Building	Process	Geneous Effluent	Type Filter Control
313	Slug Pickla	mo2, hno3	Scrubber
313	Fuel Eloment Etch Machines	по ₂ , кно ₃	Scrubber
313	Sleave Machines	Haoh, Haalo ₂	None
313	Slug Recovery	NaOH Spruy	Scrubber
313	Acid Weutralization	жо2, нко3	Scrubber
313	Spire Etch	NaOH, NaAlO2	llone
313	Special Products	NiOH Spray, Methanol Trichlorethylena	Xone
313	Cap and Can Hachines	NaOil Spray, Methanol	None
313	Rail Degreasor	Trichlorethylene	None
313	Anodising	MaON Spray Oxalic Acid Spray	Scrubber
306		ro2, mro3	Berubber
384	• • •	Combustion Products	Regenerative Fly Ash Collector
3726		Mach MC1 MMC3 Miscl M3PC4 Miscl	Scrubber .
3720	• • •	HP H280k HaCH Urasium HH3CK Thoria HHC3 Be	Particulate Filters
3732	• • •	270.5	Particulate Filter UNCLASSIFIED

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V. CONFORMANCE WITH EFFLUENT CONTROL STANDARDS

A. LIQUID EFFLUENTS

 Current practices that satisfy the intent of Executive Order 11288 include:

. SECONDARY TREATMENT

The existing process ponds, septic tanks, and leaching tranches provide the necessary secondary treatment.

. STORAGE FACILITIES

Storage facilities for liquid chemicals as presently located (See Figure 1) would not contribute a significant amount of water pollution in the Columbia River should rupture or accidental drainage occur. Most of the chemicals would be discharged to the ground. The small amount that could be expected to reach the process sewer would not be significantly greater than is currently being routinely dumped to the ponds from the various process operations in the 313 and 306 Buildings.

REVIEW AND SURVEILLANCE PROGRAMS

Weekly effluent samples at the north process pond inlet and east bank have been collected since November, 1966, by Battelle Northwest and analyzed by the DUN Analytical Laboratory. The typical range of contaminants is shown in Table IV. Notice that of those contaminants analyzed in the east bank samples only Cr^{+6} , NO₃, and F concentrations exceed the drinking water standards of 0.05, 45, and 0.8 ppm, respectively, as shown in Appendix III.

In order to provide additional information concerning the mobility of liquid effluents, a daily grab sample was collected during April, 1967, at three different locations of the north process pend - the inlet; north trough, and east bank. During periods of low river flow, river bank seepage samples were also collected and analyzed to determine the seepage concentrations of Cr^{TD} and NO3. Uranium and some fluoride analyses on certain samples were also included in order to compare the results with uranium accountability losses and determine if the NNO3-NF etch used by N-Fucls on zircally was contributing any fluoride to the river. The results of the sampling program are listed in Tables V and VI and are proceed against time in Figures 5 through 10.

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TABLE JY

Renge of Typical Contaminants

Process Pond Inlet and East Bank

Contaminant	Inlet (ppm)	East (ppm)
Copper	ND - 0.12	0.002 - 0.11
Iron	ND - 5.9	ND - 0.12
Sulfate	8 - 1890	14 - 60
Nitrate	74 - 2484	88 - 286
Chloride	0.6 - 24.0	0.5 - 9.2
Chromium (VI)	0.001 - 200	0.01 - 7.0
Zinc	<0.001 - <0.001	<0.001 - <0.001
Uranium	0.01 - 3.3	0.03 - 1.6
Fluoride	-	3.5 - 26

ND = Not Detectable

A. LIQUID EFFLUENTS (continued)

In reviewing the results of the sampling program, it is important to realize that considerable fluctuation is expected because of the various disposal frequencies of the 300-Area contractors. There is special significance in two of the graphs. Figure 10 illustrates that most of the uranium, as expected, settles out in the vicinity of the inlet, seeps through the soil and enters the river in concentrations significantly higher than those found on the east bank. Since the average inlet uranium concentration of 0.45 ppm is only slightly higher than the average bank seepage concentration of 0.36 ppm, it is believed that very little of discharged uranium is being retained by the soil. These concentrations indicate that approximately seventeen pounds of uranium per day are being discharged to the river from the 300-Area operations. This

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TABLE V

North	Process	Pond	Analyses	(mm)

Date		Inlet	•		Troug	<u>.</u>	********	E	ut_	
MARCH	ā	NO3	Cr+6	<u>u</u>	NO3	<u>Cr</u> +6	<u>v</u>	NO3	Cr+6	7
27	.11	345	-17	.09	52	.03	.07	120	.15	_
28	.68	83	.32	.13	96	.07	.11	148	•13	
29	.27	87	.25	.16	194	.08	.13	165	.11	
30	• 52	119	.68	.16	186	3.20	.04	161	3.00	•
31	.17	167	.26	.11	179	.61	.05	140	1.20	
APRIL										
3	.60	201	.28	.11	125	.04	.16	370	.18	
3 4	.11	116	.25	.13	189	.08	.18	212	.09	
5 6	.34	92	.25	.11	138	.13	.27	154	.16	
6	.16	109	. 30	.21	157	.06	.19	193	.17	
7	.19	157	1.00	.16	315	.15	.13	222	20	
10	.11	148	.21	.07	116	.03	.14	154	.11	
11	. 44	89	.22	.29	149	.07	.05	102	.08	
12	.18	93	.22	.03	316	.08	.07	140	.09	
13	.55	100	.38	.22	1.65	.05	.05	141	.07	
14	-97	169	45.60	.22	278	.03	.03	195	.03	
17	.31	104	. 30	30.	125	.31	.11	91	.60	
18	1,00	160	.22	. 52	179	.11	.01	88	.60	
19				_						
20	1.00	145		.16	240	-40	.22	145	.43	
21 24	.18	181	.22	•06	228	.22	.04	166	.68	
	.88	71,	.20	.02	86	.06	.60	138	.21	
25 26	.58	221	•35	-01	153	.23	.08	114	,21	
	1.80	6228	.02	.02	11.9	.20	.08	185	.25	
27 28	.40	293	.20	.07	385	.08	.09	333	.12	
20	.20	25 7	.18	.04	245	.11	.20	269	.11	
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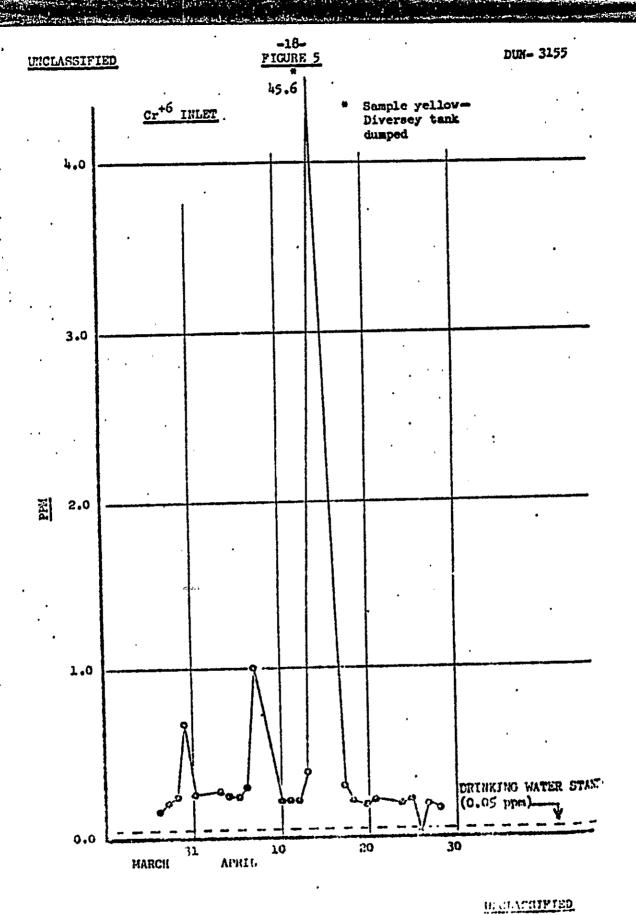
TABLE VI

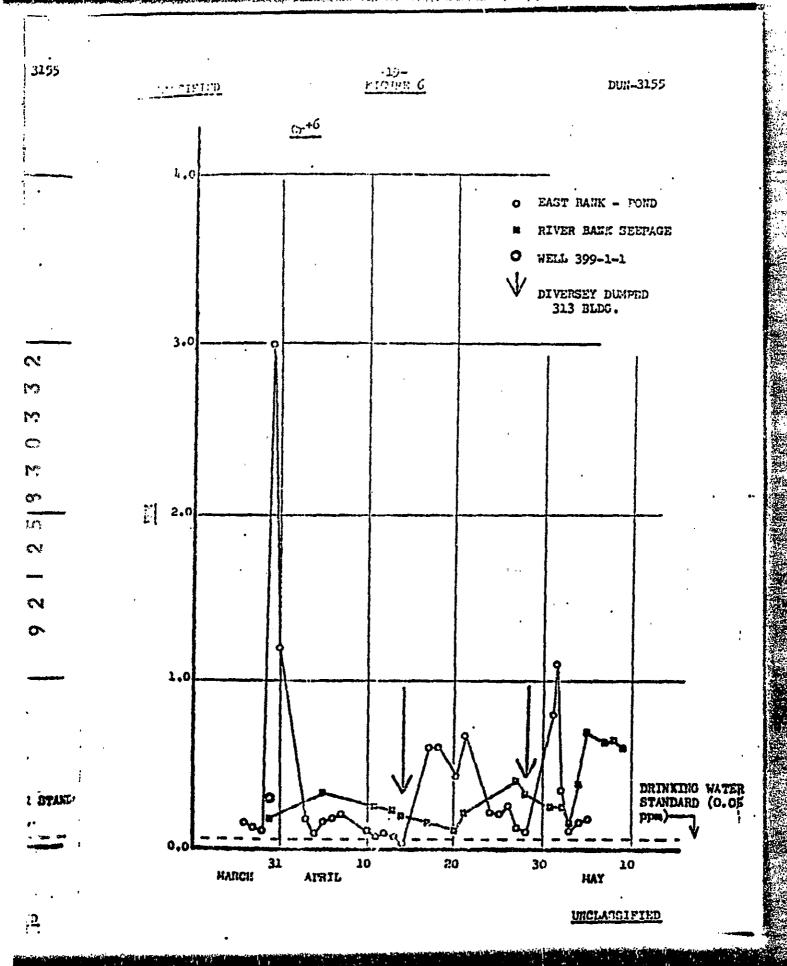
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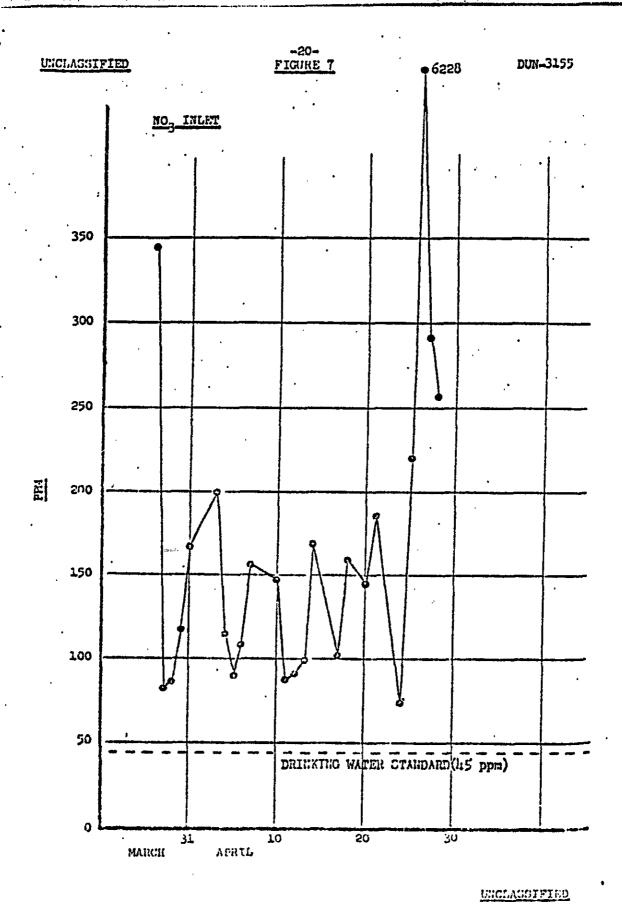
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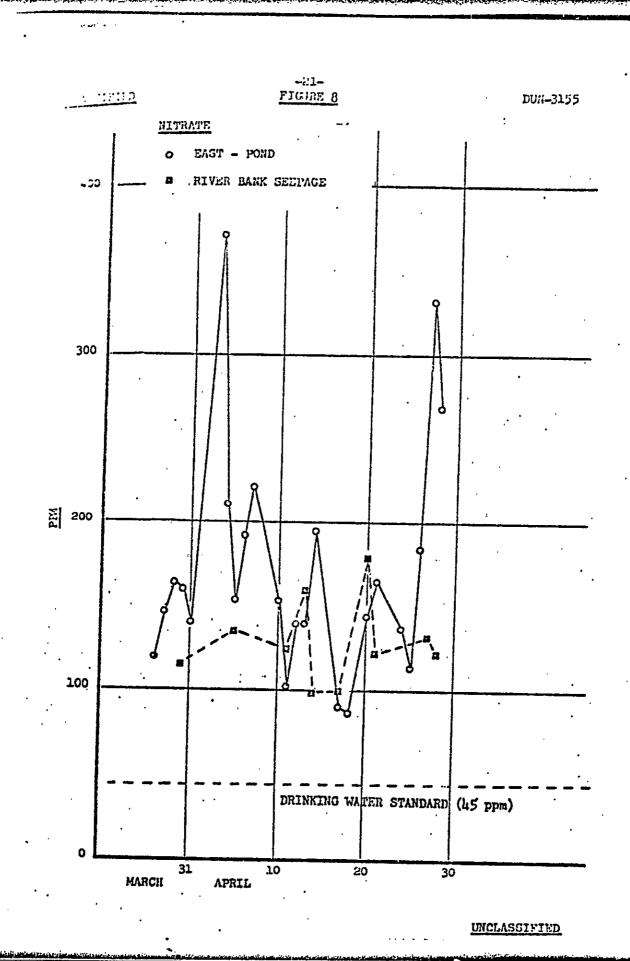
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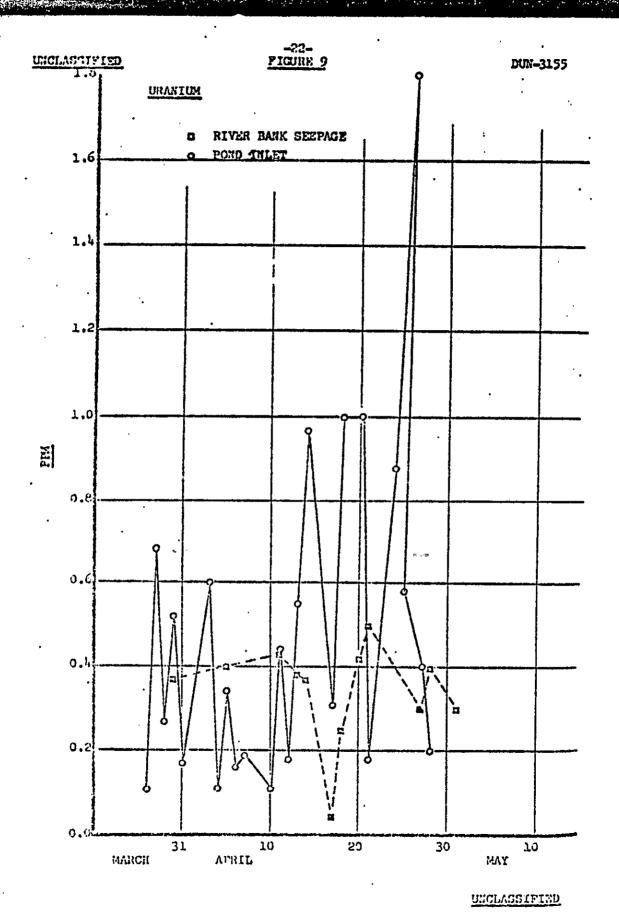


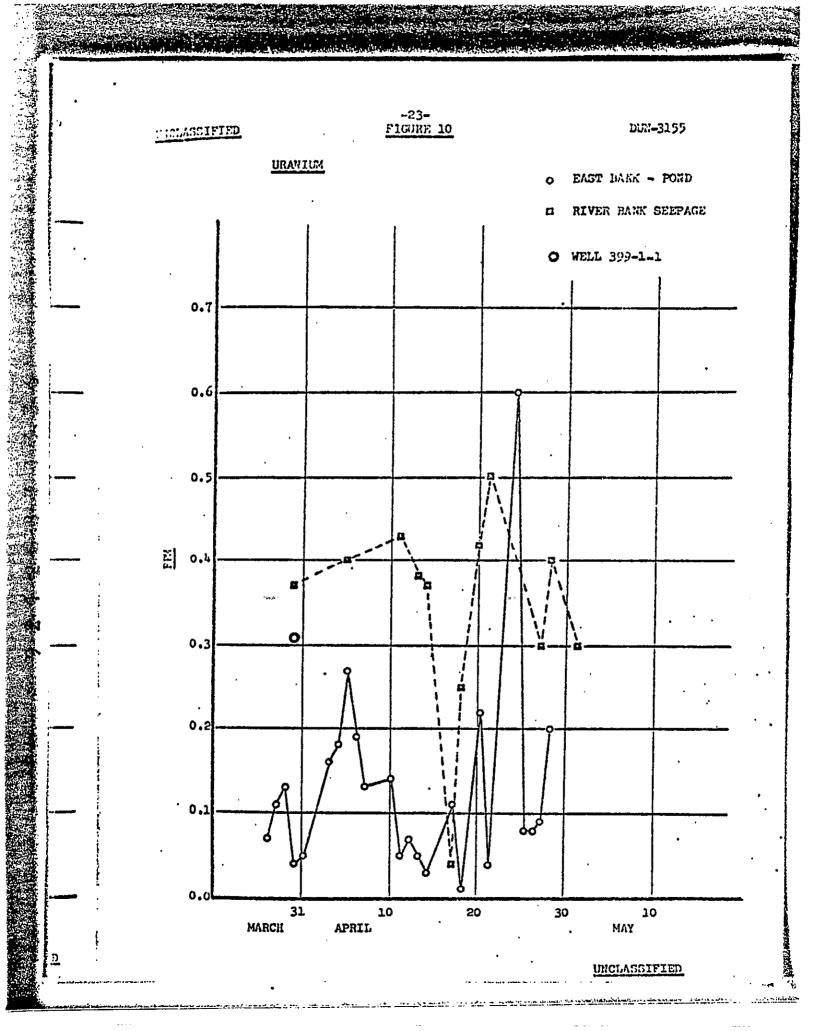






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A. LIQUID EFFLUENTS (continued)

amount of uranium does not contribute measurable human exposure and does not constitute a pollution problem.

The decxidizer solution from the component cleaning area was identified as the source of the hexavalent chromium noticed in the pond and at the river bank (see Figure 6). After each deoxidizing solution was dumped, a "wave" of Cr+6 was generated which reached the river bank some six to seven days later. The concentration rose to a peak of 0.4 ppm and slowly descended approaching the 0.05 ppm limit, but rose sgain after another deoxidizer tank was dumped. The April 28th, 1967, drain has special significance in this interpretation in that the valve on the process tank was inadvertently left open and a double batch was dumped. Notice that the concentration on the river bank increased significantly (0.7 ppm) after this incident. Although not a significant pollution problem, ways of reducing the source of Cr+6 are being investigated. Included are reduction to Cr+3 and pumping to 303-F for controlled discharges each day to the sewer. While these concentrations are above the drinking water stendard, samples taken by Battolle-Northwest at the Richland Water Plant show an average concentration of 0.008 ppm which is well below the 0.05 ppm limit for drinking water.

Fluctuation of the nitrate content makes any interpretation of the nitrate analyses difficult in regard to scepage rates and major source identification; but, on the average, the bank scepage concentrations (135 ppm) exceed the drinking water standard. Samples taken by Battelle-Northwest indicate a nitrate content less than 1 ppm in Columbia River water at the Richland Water Plant which also is much below the 45 ppm limit for drinking water.

The fluoride analyses indicate that this area should be studied further since two high readings were seen - a 26 ppm concentration in the east bank sample on May 4, 1967, and a resulting 10 ppm concentration in the bank acepage sample of May 7, 1967. Unfortunately, earlier samples were discarded before it was realized that fluoride analyses might be desirable.

Samples from the anodizing specer cleaning tank were analyzed monthly for radiochemical elements. A typical analysis is shown in Table VII. Previous samples have indicated a maximum alpha activity of 1.0 X 10⁻⁵ microcuries per milliliter and a maximum beta activity of 1.9 X 10⁻⁶ microcuries per milliliter.

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A. LIQUID EFFLUENTS (continued)

While the maximum beta activity exceeds the limit of 5 X 10⁻⁵ microcuries per milliliter permitted by RL Manual Appendix 0510, sufficient dilution is realized before the contaminants enter the process pond. Radiochemical analysis of samples taken from the north process pond, well 399-1-1, and Columbia River scepage (Table VIII) have shown a maximum total beta activity of 2.8 X 10⁻⁷ microcuries per milliliter. It is assumed that the alpha activity is also in this range with neither activity level constituting a pollution problem.

TABLE VII

Typical Radiochemical Analysis of Anodizing Caustic Solution

Isotope	Activity Loyel (pc/ml)
2n ⁶⁵	0.19
Zr-No	0.09
8e ¹⁴⁶	0.27
Fe ⁵⁹	0.03
co ⁶⁰	0,02
Co ⁵⁸	Trace
Maximum Beta	1.9 X 10 ⁻¹
Maximum Alpha	1 x 10 ⁻⁵

TABLE VIII

Typical Radiochemical Analysis of Well 399-1-1 and Bank Scepage Samples

Isotope	Bank Activity Level (µc/ml)	Well 399-1-1 Activity Level (uc/ml)
_{Zդ} 65	9.1 x 10 ⁻⁸	9.1 x 10 ⁻⁸
Co ⁶⁰	8.8 x 10 ⁻⁸	8.7 x 10 ⁻⁸
Cr ⁵¹	9.1 X 10 ⁻⁷	1.4 x 10 ⁻⁶

TADLE YIII (continued)

Inotope	Bunk Activity Level (sc/al)	Well 199-ini totivity lovel (se,
10 239	5.6 x 10 ⁻⁵	5.7 × 10 ⁻⁵
Maximus Seta	2.8 x 10 ⁻⁷	2.1 × 10 ⁻⁷

A study node by A. B. Johnson (1) indicated that redicative nativation product buildup is not to be enticipated in the process sever system because of the periodic releases of the caustic classing solution. Samples will continue to be taken in order to assure control of these releases. In addition, Enttello-Corthwest is periodically sampling the wells in the vicinity of the pends in order to assess the magnitude of radio-chemical contamination flowing to the river.

Samples have been taken from the leaching troaches and the river, both above and below the trenches, by Battolie-Horthwest and analysed for coliform content and biochemical coygen demand (BOD). A typical analysis is shown in Table IX. (For a further explanation of coliform and BOD and their relationship to water pollution, see Appendix III.) Encod on these analyses, the 300-Area sanitary waste treatment system is judged to be performing an adequate secondary treatment of soultary wastes.

Bacteriological Analysis of Leaching Trenches.
Halls, and Columbia River

Date	Invation	Coliform/100 ml	000, er/1
2/16/67	Leach Trench	60,750	28
	Will 300-1-3	20	Ö
	Well 322-3-1	120	0
3/14/67	Leach Trench	82,000	4.9
•	Well 355-1-3	75	0
	Wall 309-3-1	9	Ö
5/19/67	Leach Trench		
	Herd End	22,500	15.8
	hiver End	31,000	18.6
	River		
	Upatrenn	3.5	3.7
	Suspege Area	6	3.0

^{*} The numbers in percentages () refer to the last of References.

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A. Light Profittion (c stanged)

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Operating procedures inverting the receiving, storage, and distribution of liquid expelcate and their subsequent use in the process or cuttimes in lecuments NA-36056-100 REV and NA-NOS6-200 No. "Man reliaring Operation Operating Procedures, Fuels imported to particular These documents operated a current to the procedures and equipment used to control the process variables.

Specific Sections of the me Commercy are related to the control of liquid effluence and include the following:

e. Burnishe, from the and Bistribution of Liquid Chemicals [FE-3605n-12.70.4]

Beetlen	Irnredure
150	Yank Car sold Truck Scapling
151	Recairing, Storage, and Distribution of Mitric Acid
152	Receiving, Storage, and Distribution of Caustic
153	Receiving, Storage, and Distribution of Trichlorethylens
154	Ritrated Courtic Mixing and Distribution
155	Twonty-five Percent Sleeve Caustic Mixing and Distribution
156	Diversey 51h Solution
157	Methanol Tank Car Unloading
158	Altrex Rix and Distribution
159	Courtic Meter Operation

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OPERATING PROCEDURES (continued)

b. Use and Discharge of Liquid Wastes

Section	Procedure	
	Recovery (HW-3E058-100 REV)	
130	Stripping Tank Equipment	
131	Stripping Operation	
132	Treating Tank Equipment	
133	Treating Operation	
134	Operation of Centrifugal Pumps	
136	Spent 50% Caustic Transfer	
137	Neutralizing Process Equipment	
138	Neutralizing Process Operation	
139	Pressure Tank Equipment	
140	Pressure Tank Operation	
141	Filter Press Equipment	
142	Filter Press Operation	
<u>P1</u>	ckle Machine Operation (Hd-35058-200 REV)	
225	Pickle Machine Startup	
226	Pickle Machine Operation	
228	Pickle Machine Equipment	
229	Pickle Degrasser Still Startup	
230	Pickle Degreeser Still Operation	
231	Degresser Still Equipment	
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OPERATING PROS. DURES (continued)

	Sic. ve Enchine Congration (b3002 Size Bod)
2110	Sleave Cleaning Machine Startup
241	Sleave Classing Machine Operation
242	Slacve Cleaning Machine Fquipment
243	Sloove Cleaning Machine Eclution Makeup
g	ap and Can Muchine Operation (1:4-38-56-60- Env)
250	Cap and Can Machine Startup
251	Cap and Can Machine Operation
252	Cap and Can Machine Equipment
253	Cap and Can Cleaning Machine Solution Makeup
254	Cap and Cam Machine Safety Protection
256	Cap and Can Degresser Still Startup
- 257	Cap and Can Degresser Still Equipment
258	Methanol Still Startup

2. Future action to assure continuing compliance with Executive Order 11258 includes:

Methanol Still Operation

Methanol Still Equipment

SAMPLING PROGRAMS

259

260

On July 17, 1967, an automatic sampler was located at the 300-Area north process pond to gather a composite sample of aqueous effluents discharged from the 300-Area operations. Chemical and radiochemical analyses will be periodically performed in order to maintain a continuing inventory of

BAKPLING PROGRAMS (continued)

possible pollutants. A description of the sampler and its operating characteristics is shown in Appendix IV.

In addition to the pond samples, periodic grab samples are taken at the wells in the vicinity of the pends along with bank seepage samples whomever river conditions permit.

Samples will continue to be taken of the emodising caustic cleaning solution, and the results will be recorded and periodically reported in order to maintain continuing cognisance of this disposal activity.

Battella-Morthwest will continue to sample the leaching trenches and river for BOD and coliform content. These results will be periodically supplied to DUM.

REVIEWS

Periodic reviews of operating procedures and practices involving effluent control will be performed to insure continuing compliance with established release criteria. Quality Control will be responsible for coordinating future replies to effluent control practices.

B. GASEOUS EFFLUENTS

COMBUSTION OF FUELS

In conjunction with the compliance with Executive Order 11282, HEHF was requested to sample the 38% building powerhouse stack in order to measure the emission density of the smoke and the concentration of sulfur dioxide and recommend a detector or alarm system to monitor releases from the combustion units. The results of this sampling program have been reported by HEHF (2). Certain difficulties were encountered in obtaining representative stack gas samples because of the lack of available sample lines and particle size analysis was not made. Air samples were collected from the 150-foot stack and compared with the theoretical emission rate based on power level. At a steam generation level of 25,000 - 27,000 pounds per hour, the theoretical S02 concentration by use of fuel consumption is 214 ppm. The sample showed a concentration of 143 ppm.

By the use of curves comprised of ambient air concentrations versus meteorological parameters as related to stack gas sources, and assuming a study load of 50,000 pounds per hour, a stack emission of 1.7 X 10⁻³ cubic meters of 50g per second

COMMUSTION OF THE Continued)

would result. Estimated ground level concentrations extrapolated from mateoreing each curven would be less than 0.1 ppm at 4,000 maters under stable atmospheric conditions and 5.0 ppm at 60 to 70 meters under santable atmospheric conditions. Because the boilers that are normally operated during high stams generation (50,000 to 125,000 pounds of steam per hour) were not operating during the study, it appears that the on-site ground concentrations of 60g could be of cencers. For this reason, supplementary studies will be made during the winter months when high steam generation rates are expected.

Studies have shown that a concentration of 0.6 ppm of SO₂ will produce no datactable response in healthy human beings; but in the range between 1 and 5 ppm, nost persons will begin to show a detectable response (3). There is no sound evidence that chronic exposure to concentrations below 5 ppm of SO₂, by itself, has any persistently ill effects. Nost people can detect 5 ppm, and it produces a distinctive gross physiological response — exposure for one hour causes choking. Most people find 10 ppm quite unpleasant; an exposure for one hour to this concentration produces severe distress.

It appears from the mathematical model used by HEHF that concentrations of greater than 5 ppm could be found at ground level during high generation, and it could be that certain controls will have to be implemented should this turn out to be the case.

Smoke density measurements made with a Mines Safety Appliance Smokescope showed that the density of the smoke was below shade number one on the Ringelmann Scale and, therefore, complies with the standard. Since the smoke density complies with the standard, it is believed that the particle size emission is also below the allowable release level. Measurement of particle size would be very difficult, and HEHF feels that it is no problem.

It is interesting to note that when the size of particles in an exhaust stream approaches the wave length of light, the stack discharge is quite visible in spite of the fact that the actual quantity of particles may be small. Thus, since visibility of an effluent exhaust is a function of the light-reflecting surfaces of the escaping material and since surface area per pound increases inversely with the square of the particle size, it is possible to remove 80 to 90 percent of the material from an exhaust stack without altering its appearance (4).

CONBUSTION OF FUELS (continued)

The recommendation from HEHF as to the type of sacks alarms for monitoring the combustion units is pending until a reply to an inquiry to the Department of Health, Education, and Walfare is received.

DISPOSAL OF REPUSE

Current disposal practices do not conform to the daily limit of 25 pounds of material that can be burned in open pits; but because of the remote location, low population density, refuse being primarily paper, and favorable meteorological conditions, it is believed that this standard is unduly restrictive, and an exemption has been requested by the RL-AEC. In conjunction with the dark-smoke-producing requirement, all subsections within the Production Fuels Section have been informed that should significant quantities of this material be generated, special disposal procedures should be used.

OTHER POLLUTION-FRODUCING PROCESSES

HEHF has sampled the stacks in the 313 and 306 buildings and has issued a report on the concentrations of gaseous effluents (5). The results indicate that scrubber replacements should be considered (see Appendix VIII for diagrams of current scrubber systems).

HEHF is scheduled to procure air monitoring equipment in October, 1967, and will monitor selected locations in the 300 Area to determine if the Production Fuels Section's gaseous effluents are harmful. Until that time, no change in the current mode of operation is contemplated.

RADIOACTIVITY

Previous investigation has shown that the Production Fuels Section does not contribute any gaseous radioactive effluents to the atmosphere that would be considered as harmful or hazardous to the public (6).

TI. RECORDS AND REPORTING

A. LIQUID EFFLUENT SAMPLES

Chemical and radiochemical analytes of the 300-Area process effluents will be reported monthly in the Quality Control Record Report. Significant changes will be descussed along with the planned action of reduction of the concentrations of those contaminants which are convidered potential pollution contributors. The analyses will be supplied to these persons responsible for preparing the DUN Annual Report on Pollution Control Practices.

Summaries of the coliform and BOD content of leaching trenches and Columbia River samples will be reported when received from Battelle:

Semiannual radioactive waste disposed reports will be prepared based on the requirements of RL-0500.

B. GASEOUS EFFLUENTS

NEWF will be periodically sampling at different locations in the 300 Area starting in October, 1967. The results of these sampling programs will be documented and distributed to those concerned with this program. A sementual gaseous effluent analysis of the Production Fuels Section buildings will be made and documented. Based on the results of these analyses, recommended changes will be offered in order to assure continuing compliance. The results of these various sampling programs, likewise, will be supplied to those responsible for conducting the annual DUN report on gaseous effluent control and the semi-annual radioactive disposal report.

VII. ACKNOWLEDGMENTS

Appreciation is extended to C. D. Corbit for his review and suggestions and to C. T. Houghan for his effort in supplying the graphs and drawings.

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